

JAN 6 1997

RESERVE DESK

Day 3 - Reactor Engineering and
Design (Fission Option)
Ph.D. Qualifying Exam
Fall Quarter 1996 - Page One

GEORGIA INSTITUTE OF TECHNOLOGY

The George W. Woodruff
School of Mechanical Engineering

NUCLEAR ENGINEERING

Ph.D. Qualifiers Exam - Fall Quarter 1996

Reactor Engineering and Design (Fission Option)

EXAM AREA

Assigned Number **(DO NOT SIGN YOUR NAME)**

-- Please sign your name on the back of this page --

GEORGIA INSTITUTE OF TECHNOLOGY

The George W. Woodruff School of Mechanical Engineering

Nuclear Engineering

Ph.D. Qualifiers Exam

Fall Quarter, 1996

Day 3

Instructions

1. Complete 6 of the 10 questions **PLUS THE "DESIGN PROBLEM"**.
2. Place your identifying code letter on the top right corner of each page of your question and answer sheets.
3. Use a separate page for each answer sheet (no front to back answers).
4. The question number should be shown on each answer sheet.
5. Staple your question sheet to your answer sheets and turn in.

NE.III.1. For incompressible, fully-developed laminar flow in a circular tube the velocity profile is:

$$u(r) = 2u_m \left[1 - \left(\frac{r}{r_o} \right)^2 \right]$$

where

- u = velocity
- r = radial coordinate
- r_o = tube radius
- u_m = average velocity

The energy conservation equation, furthermore, for a constant heat flux boundary condition can be represented as:

$$u \frac{dT_m}{dz} = \frac{\alpha}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right)$$

where T_m = average temperature.

Prove that

$$Nu = \frac{2 h r_o}{k} = \frac{48}{11}$$

NE.III.2. Among the current areas of interest in waste management today is the nondestructive assay of containers which contain ^{239}Pu .

- a. If a neutron detector were to be placed at a container having small amounts of ^{239}Pu in it, would it record any neutron counts from the container?
- b. If a steady-state neutron source, such as ^{252}Cf (fission spectrum), is placed next to the container, how might we use the count rate recorded by the neutron detector to assay the plutonium content or, if you rather, the value of k_{eff} for the container.
- c. Would a pulsed neutron source offer any advantage over a steady-state one?
- d. Would a thermal-neutron or a fast-neutron detector yield more information?
- e. Could a gamma-ray detector give you any additional information?

NE.III.3. A PWR secondary plant uses U-tube steam generators in a regenerative-reheat Rankine cycle with moisture separation. The feedwater line contains a sequence of three closed feedwater heaters. The drain for the lowest pressure feedwater heater is pumped forward, while the drains for the other two heaters are cascaded backward.

- a. Draw a schematic diagram of the secondary plant showing all components and their interconnections.
- b. Label all states on the system diagram in part "a" above and show them on the corresponding T-s diagram for the cycle. Assume all turbines and pumps to be non-ideal.

- NE.III.4. a. Describe the gaseous diffusion process for enriching uranium. What is the theoretical separation per stage of the gaseous diffusion process? What determines it?
- b. NUEXCO reported in early 1989 that the cost of U_3O_8 was \$11.60/lb, UF_6 conversion \$34.75/kg, and enrichment \$67/kg-SWU. Estimate the cost for 1 kg of 3% enriched uranium.
- c. The reported end-of-year prices in 1989 were \$9/lb, \$26.50/lb, and \$54/kg-SWU, respectively. Compare the price of 1 kg of 3% enriched uranium to the price you calculated in (b).

Some equations: (subscripts: f = feed, p = product, t = tails)

$$\frac{M_f}{M_p} = \frac{p - t}{f - t}$$

$$V(x) = (2x - 1) \ln \left(\frac{x}{1 - x} \right)$$

$$f = \alpha^n$$

- NE.III.5. a. Derive the void-quality relation for one-dimensional homogeneous flow and separated-flow models.
- b. According to the Drift Flux Model (DFM), void fraction in a channel can be found from:

$$\alpha = \frac{j_G}{C_0 j + V_{Gj}}$$

where

- α = void fraction
- j = total superficial velocity
- j_G = gas superficial velocity
- C_0 = DFM distribution coefficient
- V_{Gj} = gas drift velocity

Derive the DFM void-quality relation (i.e., a relation between void fraction, α , and quality, x , which involves DFM parameters, phase densities and the total mass flux, G).

NE.III.6. A large iron plate 30-cm thick is subjected to pure gamma radiations from both sides. On one side it is subjected to 10^{14} γ -flux of 3.0 Mev/photon energy; on the other side it is subjected to 10^{13} γ -flux of 1.0 Mev/photon energy. Both surfaces of the plate are held at 250 °C. Assuming no interaction between the radiations and no buildup factor; find:

- a. The magnitude and location of the maximum temperature within the slab.
- b. The surface heat flux for both sides of the slab.

[For iron: density = 7.86 g/cc; thermal conductivity = 59 W/m°C; absorption coefficient for 1.0 Mev gamma = 0.470 cm^{-1} ; absorption coefficient for 3.0 Mev gamma = 0.282 cm^{-1}]

NE.III.7. Compare properties of metallic uranium and uranium oxide and explain the reasons for choosing uranium oxide as a nuclear fuel in most power-generating nuclear reactors. Describe the changes in the structure of the uranium oxide pellets during the operation of a nuclear reactor and the interaction between the pellets and the cladding.

NE.III.8. Explain the choice of materials for the pressure vessels of Boiling Water Reactors and Pressurized Water Reactors (BWRs and PWRs). List the main requirements and discuss the changes in the important properties as a result of neutron irradiation.

NE.III.9. A natural internal recirculation BWR operates at an average pressure of 1000psia. The average densities in the nonboiling and boiling heights are 47 and 38 lbm/ft³, respectively. These heights are 2.0 and 3.0 ft, respectively. The downcomer temperature is 520 °F, while the core average exit quality is 8 percent. The total pressure losses in the downcomer, core and chimney are 0.527 psi. Assuming a slip ratio of 2.0, determine the necessary chimney height in feet. List all assumptions. (Attached two sheets)

Table 2: Saturated Steam: Pressure Table

Abs. Press. Lb/Sq In p	Temp Fahr t	Sat. Liquid v _f	Specific Volume		Sat. Vapor v _g	Enthalpy			Entropy			Abs. Press. Lb/Sq In p
			Evap v _{fg}	Sat. Vapor v _g		Sat. Liquid h _f	Evap h _{fg}	Sat. Vapor h _g	Sat. Liquid s _f	Evap s _{fg}	Sat. Vapor s _g	
0.00065	32.018	0.016022	3302.4	3302.4	0.0003	1075.5	1075.5	0.0000	2.1872	2.1872	0.00065	
0.25	59.323	0.016032	1235.5	1235.5	0.0003	1060.1	1087.4	0.0542	2.0425	2.0967	0.25	
0.50	79.586	0.016071	641.5	641.5	0.0003	1048.6	1096.3	0.0925	1.9446	2.0371	0.50	
1.0	101.74	0.016136	333.59	333.60	0.0003	1036.1	1105.8	0.1326	1.8455	1.9781	1.0	
5.0	162.24	0.016407	73.515	73.532	0.0003	1000.9	1131.1	0.2349	1.6094	1.8443	5.0	
10.0	193.21	0.016592	38.404	38.420	0.0003	982.1	1143.3	0.2836	1.5043	1.7879	10.0	
14.696	212.00	0.016719	26.782	26.799	0.0003	970.3	1150.5	0.3121	1.4447	1.7568	14.696	
15.0	213.03	0.016726	26.274	26.290	0.0003	969.7	1150.9	0.3137	1.4415	1.7552	15.0	
20.0	227.96	0.016834	20.070	20.087	0.0003	960.1	1156.3	0.3358	1.3962	1.7320	20.0	
30.0	250.34	0.017009	13.7266	13.7436	0.0003	945.2	1164.1	0.3682	1.3313	1.6995	30.0	
40.0	267.25	0.017151	10.4794	10.4965	0.0003	933.6	1169.8	0.3921	1.2844	1.6765	40.0	
50.0	281.02	0.017274	8.4967	8.5140	0.0003	923.9	1174.1	0.4112	1.2474	1.6586	50.0	
60.0	292.71	0.017383	7.1562	7.1736	0.0003	915.4	1177.6	0.4273	1.2167	1.6440	60.0	
70.0	302.93	0.017482	6.1875	6.2050	0.0003	907.8	1180.6	0.4411	1.1905	1.6316	70.0	
80.0	312.04	0.017573	5.4536	5.4711	0.0003	900.9	1183.1	0.4534	1.1675	1.6208	80.0	
90.0	320.28	0.017659	4.8779	4.8953	0.0003	894.6	1185.3	0.4643	1.1470	1.6113	90.0	
100.0	327.82	0.017740	4.4133	4.4310	0.0003	888.6	1187.2	0.4743	1.1284	1.6027	100.0	
110.0	334.79	0.01782	4.0306	4.0484	0.0003	883.1	1188.9	0.4834	1.1115	1.5950	110.0	
120.0	341.27	0.01789	3.7097	3.7275	0.0003	877.8	1190.4	0.4919	1.0960	1.5879	120.0	
130.0	347.33	0.01796	3.4364	3.4544	0.0003	872.8	1191.7	0.4998	1.0815	1.5813	130.0	
140.0	353.04	0.01803	3.2010	3.2190	0.0003	868.0	1193.0	0.5071	1.0681	1.5752	140.0	
150.0	358.43	0.01809	2.9958	3.0139	0.0003	863.4	1194.1	0.5141	1.0554	1.5695	150.0	
160.0	363.55	0.01815	2.8155	2.8336	0.0003	859.0	1195.1	0.5206	1.0435	1.5641	160.0	
170.0	368.42	0.01821	2.6556	2.6738	0.0003	854.8	1196.0	0.5269	1.0322	1.5591	170.0	
180.0	373.08	0.01827	2.5129	2.5312	0.0003	850.7	1196.9	0.5328	1.0215	1.5543	180.0	
190.0	377.53	0.01833	2.3847	2.4030	0.0003	846.7	1197.6	0.5384	1.0113	1.5498	190.0	
200.0	381.80	0.01839	2.2689	2.2873	0.0003	842.8	1198.3	0.5438	1.0016	1.5454	200.0	
210.0	385.91	0.01844	2.1637	2.1821	0.0003	839.1	1199.0	0.5490	0.9923	1.5413	210.0	
220.0	389.88	0.01850	2.0677	2.0862	0.0003	835.4	1199.6	0.5540	0.9834	1.5374	220.0	
230.0	393.70	0.01855	1.9791	1.9986	0.0003	831.8	1200.1	0.5588	0.9748	1.5336	230.0	
240.0	397.39	0.01860	1.8990	1.9185	0.0003	828.4	1200.6	0.5634	0.9665	1.5299	240.0	
250.0	400.97	0.01865	1.8245	1.8431	0.0003	825.0	1201.1	0.5679	0.9585	1.5264	250.0	
260.0	404.44	0.01870	1.7548	1.7734	0.0003	821.6	1201.5	0.5722	0.9508	1.5230	260.0	
270.0	407.80	0.01875	1.6913	1.7101	0.0003	818.3	1201.9	0.5764	0.9433	1.5197	270.0	
280.0	411.07	0.01880	1.6319	1.6509	0.0003	815.1	1202.3	0.5805	0.9361	1.5166	280.0	
290.0	414.25	0.01885	1.5759	1.5948	0.0003	812.0	1202.6	0.5844	0.9291	1.5135	290.0	
300.0	417.35	0.01889	1.5238	1.5427	0.0003	808.9	1202.9	0.5882	0.9223	1.5105	300.0	
350.0	431.73	0.01912	1.3064	1.3254	0.0003	794.2	1204.0	0.6059	0.8909	1.4968	350.0	
400.0	444.60	0.01934	1.1416	1.1609	0.0003	780.4	1204.6	0.6217	0.8630	1.4847	400.0	
450.0	456.28	0.01954	1.0122	1.0317	0.0003	767.5	1204.8	0.6360	0.8378	1.4738	450.0	
500.0	467.01	0.01975	0.9078	0.9272	0.0003	755.1	1204.7	0.6490	0.8148	1.4639	500.0	
550.0	476.94	0.01994	0.8218	0.8417	0.0003	743.3	1204.3	0.6611	0.7936	1.4547	550.0	
600.0	486.20	0.02013	0.7496	0.7697	0.0003	732.0	1203.7	0.6723	0.7738	1.4461	600.0	
650.0	494.89	0.02032	0.6881	0.7084	0.0003	720.9	1202.8	0.6828	0.7552	1.4381	650.0	
700.0	503.08	0.02050	0.6350	0.6556	0.0003	710.2	1201.8	0.6928	0.7377	1.4304	700.0	
750.0	510.84	0.02069	0.5880	0.6094	0.0003	699.8	1200.7	0.7022	0.7210	1.4232	750.0	
800.0	518.21	0.02087	0.5480	0.5689	0.0003	689.6	1199.4	0.7111	0.7051	1.4163	800.0	
850.0	525.24	0.02105	0.5119	0.5330	0.0003	679.5	1198.0	0.7197	0.6899	1.4096	850.0	
900.0	531.95	0.02123	0.4796	0.5009	0.0003	669.7	1196.4	0.7279	0.6753	1.4032	900.0	
950.0	538.39	0.02141	0.4506	0.4720	0.0003	660.0	1194.7	0.7358	0.6612	1.3970	950.0	
1000.0	544.58	0.02159	0.4243	0.4459	0.0003	650.4	1192.9	0.7434	0.6476	1.3910	1000.0	
1050.0	550.53	0.02177	0.4004	0.4224	0.0003	640.9	1191.0	0.7507	0.6344	1.3851	1050.0	
1100.0	556.28	0.02195	0.3786	0.4005	0.0003	631.5	1189.1	0.7578	0.6216	1.3794	1100.0	
1150.0	561.82	0.02214	0.3589	0.3807	0.0003	622.2	1187.0	0.7647	0.6091	1.3738	1150.0	
1200.0	567.19	0.02232	0.3401	0.3624	0.0003	613.0	1184.8	0.7714	0.5969	1.3683	1200.0	
1250.0	572.38	0.02250	0.3230	0.3456	0.0003	603.8	1182.6	0.7780	0.5850	1.3630	1250.0	
1300.0	577.42	0.02269	0.3072	0.3299	0.0003	594.6	1180.2	0.7843	0.5733	1.3577	1300.0	
1350.0	582.32	0.02288	0.2925	0.3153	0.0003	585.4	1177.8	0.7906	0.5620	1.3525	1350.0	
1400.0	587.07	0.02307	0.2787	0.3017	0.0003	576.5	1175.3	0.7966	0.5507	1.3474	1400.0	
1450.0	591.70	0.02327	0.2658	0.2891	0.0003	567.5	1172.8	0.8026	0.5397	1.3423	1450.0	
1500.0	596.20	0.02346	0.2537	0.2771	0.0003	558.4	1170.1	0.8085	0.5288	1.3373	1500.0	
1550.0	600.59	0.02366	0.2423	0.2660	0.0003	549.4	1167.4	0.8142	0.5182	1.3324	1550.0	
1600.0	604.87	0.02387	0.2315	0.2554	0.0003	540.3	1164.5	0.8199	0.5076	1.3274	1600.0	
1650.0	609.05	0.02407	0.2214	0.2451	0.0003	531.3	1161.6	0.8254	0.4971	1.3225	1650.0	
1700.0	613.13	0.02428	0.2117	0.2360	0.0003	522.2	1158.6	0.8309	0.4867	1.3176	1700.0	
1750.0	617.12	0.02450	0.2026	0.2271	0.0003	513.1	1155.6	0.8363	0.4765	1.3128	1750.0	
1800.0	621.02	0.02472	0.1939	0.2186	0.0003	503.8	1152.3	0.8417	0.4662	1.3079	1800.0	
1850.0	624.83	0.02495	0.1858	0.2105	0.0003	494.6	1149.0	0.8470	0.4561	1.3030	1850.0	
1900.0	628.56	0.02517	0.1776	0.2027	0.0003	485.2	1145.6	0.8522	0.4459	1.2981	1900.0	
1950.0	632.22	0.02541	0.1699	0.1954	0.0003	475.8	1142.0	0.8574	0.4358	1.2931	1950.0	
2000.0	635.80	0.02565	0.1626	0.1883	0.0003	466.2	1138.3	0.8625	0.4256	1.2881	2000.0	
2100.0	642.76	0.02615	0.1488	0.1750	0.0003	446.7	1130.5	0.8727	0.4053	1.2780	2100.0	
2200.0	649.45	0.02669	0.1360	0.1627	0.0003	426.7	1122.2	0.8828	0.3848	1.2676	2200.0	
2300.0	655.89	0.02727	0.1240	0.1513	0.0003	406.0	1113.2	0.8929	0.3640	1.2569	2300.0	
2400.0	662.11	0.02790	0.1128	0.1407	0.0003	384.8	1103.7	0.9031	0.3430	1.2460	2400.0	
2500.0	668.11	0.02859	0.1020	0.1306	0.0003	361.6	1093.3	0.9139	0.3206	1.2345	2500.0	
2600.0	673.91	0.02938	0.0917	0.1211	0.0003	337.6	1082.0	0.9247	0.2977	1.2225	2600.0	
2700.0	679.53	0.03029	0.0816	0.1119	0.0003	312.3	1069.7	0.9356	0.2741	1.2097	2700.0	
2800.0	684.96	0.03134	0.0717	0.1030	0.0003	285.1	1055.8	0.9468	0.2491	1.1958	2800.0	
2900.0	690.22	0.03262	0.0615	0.0942	0.0003	254.7	1039.8	0.9588	0.2215	1.1803	2900.0	
3000.0	695.33	0.03428	0.0507	0.0850	0.0003	218.4	1020.3	0.9728	0.1891	1.1619	3000.0	
3100.0	700.28	0.03681	0.0371	0.0745	0.0003	169.3	993.3	0.9914	0.1460	1.1373	3100.0	
3200.0	705.08	0.04472	0.0191	0.0566	0.0003	56.1	931.6	1.0351	0.0482	1.0832	3200.0	
3208.2*	705.47	0.05078	0.0000	0.0507	0.0003	906.0	906.0	1.0612	0.0000	1.0612	3208.2*	

*Critical pressure

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Table 1. Saturated Steam: Temperature Table—Continued

Temp Fahr t	Abs Press Lb per Sq In p	Specific Volume			Enthalpy			Entropy			Temp Fahr t
		Sat Liquid v _f	Evap v _{fg}	Sat Vapor v _g	Sat Liquid h _f	Evap h _{fg}	Sat Vapor h _g	Sat Liquid s _f	Evap s _{fg}	Sat Vapor s _g	
460.0	466.87	0.01961	0.97463	0.99424	441.5	763.2	1204.8	0.6405	0.8299	1.4704	460.0
464.0	485.56	0.01969	0.93588	0.95557	446.1	758.6	1204.7	0.6454	0.8213	1.4667	464.0
468.0	504.63	0.01976	0.89885	0.91862	450.7	754.0	1204.6	0.6502	0.8127	1.4629	468.0
472.0	524.67	0.01984	0.86345	0.88329	455.2	749.3	1204.5	0.6551	0.8042	1.4592	472.0
476.0	545.11	0.01992	0.82958	0.84950	459.9	744.5	1204.3	0.6599	0.7956	1.4555	476.0
480.0	566.15	0.02000	0.79716	0.81717	464.5	739.6	1204.1	0.6648	0.7871	1.4518	480.0
484.0	587.81	0.02009	0.76613	0.78622	469.1	734.7	1203.8	0.6696	0.7785	1.4481	484.0
488.0	610.10	0.02017	0.73641	0.75658	473.8	729.7	1203.5	0.6745	0.7700	1.4444	488.0
492.0	633.03	0.02026	0.70794	0.72820	478.5	724.6	1203.1	0.6793	0.7614	1.4407	492.0
496.0	656.61	0.02034	0.68065	0.70100	483.2	719.5	1202.7	0.6842	0.7528	1.4370	496.0
500.0	680.86	0.02043	0.65448	0.67492	487.9	714.3	1202.2	0.6890	0.7443	1.4333	500.0
504.0	705.78	0.02053	0.62938	0.64991	492.7	709.0	1201.7	0.6939	0.7357	1.4296	504.0
508.0	731.40	0.02062	0.60530	0.62592	497.5	703.7	1201.1	0.6987	0.7271	1.4258	508.0
512.0	757.72	0.02072	0.58218	0.60289	502.3	698.2	1200.5	0.7036	0.7185	1.4221	512.0
516.0	784.76	0.02081	0.55997	0.58079	507.1	692.7	1199.8	0.7085	0.7099	1.4183	516.0
520.0	812.53	0.02091	0.53864	0.55956	512.0	687.0	1199.0	0.7133	0.7013	1.4146	520.0
524.0	841.04	0.02102	0.51814	0.53916	516.9	681.3	1198.2	0.7182	0.6926	1.4108	524.0
528.0	870.31	0.02112	0.49843	0.51955	521.8	675.5	1197.3	0.7231	0.6839	1.4070	528.0
532.0	900.34	0.02123	0.47947	0.50070	526.8	669.6	1196.4	0.7280	0.6752	1.4032	532.0
536.0	931.17	0.02134	0.46123	0.48257	531.7	663.6	1195.4	0.7329	0.6665	1.3993	536.0
540.0	962.79	0.02146	0.44367	0.46513	536.8	657.5	1194.3	0.7378	0.6577	1.3954	540.0
544.0	995.22	0.02157	0.42677	0.44834	541.8	651.3	1193.1	0.7427	0.6489	1.3915	544.0
548.0	1028.49	0.02169	0.41048	0.43217	546.9	645.0	1191.9	0.7476	0.6400	1.3876	548.0
552.0	1062.59	0.02182	0.39479	0.41660	552.0	638.5	1190.6	0.7525	0.6311	1.3837	552.0
556.0	1097.55	0.02194	0.37966	0.40160	557.2	632.0	1189.2	0.7575	0.6222	1.3797	556.0
560.0	1133.38	0.02207	0.36507	0.38714	562.4	625.3	1187.7	0.7625	0.6132	1.3757	560.0
564.0	1170.10	0.02221	0.35099	0.37320	567.6	618.5	1186.1	0.7674	0.6041	1.3716	564.0
568.0	1207.72	0.02235	0.33741	0.35975	572.9	611.5	1184.5	0.7725	0.5950	1.3675	568.0
572.0	1246.26	0.02249	0.32429	0.34678	578.3	604.5	1182.7	0.7775	0.5859	1.3634	572.0
576.0	1285.74	0.02264	0.31162	0.33426	583.7	597.2	1180.9	0.7825	0.5766	1.3592	576.0
580.0	1326.17	0.02279	0.29937	0.32216	589.1	589.9	1179.0	0.7876	0.5673	1.3550	580.0
584.0	1367.7	0.02295	0.28753	0.31048	594.6	582.4	1176.9	0.7927	0.5580	1.3507	584.0
588.0	1410.0	0.02311	0.27608	0.29919	600.1	574.7	1174.8	0.7978	0.5485	1.3464	588.0
592.0	1453.3	0.02328	0.26499	0.28827	605.7	566.8	1172.6	0.8030	0.5390	1.3420	592.0
596.0	1497.8	0.02345	0.25425	0.27770	611.4	558.8	1170.2	0.8082	0.5293	1.3375	596.0
600.0	1543.2	0.02364	0.24384	0.26747	617.1	550.6	1167.7	0.8134	0.5196	1.3330	600.0
604.0	1589.7	0.02382	0.23374	0.25757	622.9	542.2	1165.1	0.8187	0.5097	1.3284	604.0
608.0	1637.3	0.02402	0.22394	0.24796	628.8	533.6	1162.4	0.8240	0.4997	1.3238	608.0
612.0	1686.1	0.02422	0.21442	0.23865	634.8	524.7	1159.5	0.8294	0.4896	1.3190	612.0
616.0	1735.9	0.02444	0.20516	0.22960	640.8	515.6	1156.4	0.8348	0.4794	1.3141	616.0
620.0	1786.9	0.02466	0.19615	0.22081	646.9	506.3	1153.2	0.8403	0.4689	1.3092	620.0
624.0	1839.0	0.02489	0.18737	0.21226	653.1	496.6	1149.8	0.8458	0.4583	1.3041	624.0
628.0	1892.4	0.02514	0.17880	0.20394	659.5	486.7	1146.1	0.8514	0.4474	1.2988	628.0
632.0	1947.0	0.02539	0.17044	0.19583	665.9	476.4	1142.2	0.8571	0.4364	1.2934	632.0
636.0	2002.8	0.02566	0.16226	0.18792	672.4	465.7	1138.1	0.8628	0.4251	1.2879	636.0
640.0	2059.9	0.02595	0.15427	0.18021	679.1	454.6	1133.7	0.8686	0.4134	1.2821	640.0
644.0	2118.3	0.02625	0.14644	0.17269	685.9	443.1	1129.0	0.8746	0.4015	1.2761	644.0
648.0	2178.1	0.02657	0.13876	0.16534	692.9	431.1	1124.0	0.8806	0.3893	1.2699	648.0
652.0	2239.2	0.02691	0.13124	0.15816	700.0	418.7	1118.7	0.8868	0.3767	1.2634	652.0
656.0	2301.7	0.02728	0.12387	0.15115	707.4	405.7	1113.1	0.8931	0.3637	1.2567	656.0
660.0	2365.7	0.02768	0.11663	0.14431	714.9	392.1	1107.0	0.8995	0.3502	1.2498	660.0
664.0	2431.1	0.02811	0.10947	0.13757	722.9	377.7	1100.6	0.9064	0.3361	1.2425	664.0
668.0	2498.1	0.02858	0.10229	0.13087	731.5	362.1	1093.5	0.9137	0.3210	1.2347	668.0
672.0	2566.6	0.02911	0.09514	0.12424	740.2	345.7	1085.9	0.9212	0.3054	1.2266	672.0
676.0	2636.8	0.02970	0.08799	0.11769	749.2	328.5	1077.6	0.9287	0.2892	1.2179	676.0
680.0	2708.6	0.03037	0.08080	0.11117	758.5	310.1	1068.5	0.9365	0.2720	1.2086	680.0
684.0	2782.1	0.03114	0.07349	0.10463	768.2	290.2	1058.4	0.9447	0.2537	1.1984	684.0
688.0	2857.4	0.03204	0.06595	0.09799	778.8	268.2	1047.0	0.9535	0.2337	1.1872	688.0
692.0	2934.5	0.03313	0.05797	0.09110	790.5	243.1	1033.6	0.9634	0.2110	1.1744	692.0
696.0	3013.4	0.03455	0.04916	0.08371	804.4	212.8	1017.2	0.9749	0.1841	1.1591	696.0
700.0	3094.3	0.03662	0.03857	0.07519	822.4	172.7	995.2	0.9901	0.1490	1.1390	700.0
704.0	3135.5	0.03824	0.03173	0.06997	835.0	144.7	979.7	1.0006	0.1246	1.1252	704.0
708.0	3177.2	0.04108	0.02192	0.06300	854.2	102.0	956.2	1.0169	0.0876	1.1046	708.0
712.0	3198.3	0.04427	0.01304	0.05730	873.0	61.4	934.4	1.0329	0.0527	1.0856	712.0
716.0	3208.2	0.05078	0.00000	0.05078	906.0	0.0	906.0	1.0612	0.0000	1.0612	716.0

*Critical temperature

NE.III.10. Consider an LWR fueled with slightly enriched uranium. The delayed neutrons may be represented by one effective group with $\beta = 0.0075$, $\lambda = 0.08 \text{ s}^{-1}$ and $\Lambda = 6 \times 10^{-5} \text{ s}$. There is a fault signal on the control rod drive indicator and simultaneously the neutron signal increases instantaneously by a factor of 1.25 and then continues to increase. There is a manual override for the control rod system which can insert rods within five seconds and there is, of course, a scram system which will rapidly insert all the control rods. Your operational procedure requires you to scram only if the power overshoot exceeds 150% of nominal power before the manual override system can be activated. Do you scram? Explain your reasoning.

Design Problem

- NE.III.11. Suppose that you are to design an idealized light water reactor (LWR) core with the goal of obtaining the maximum energy per unit of fuel. One method of solution is to optimize (i) the neutron economy (i.e., minimize neutron loss) and (ii) the fuel utilization.
- a. In each case, identify at least one approach to optimization, ignoring the practicality of your approach (i.e. neglect heat removal, fission product containment, irradiation damage to fuel and overall plant economics). What type of core configuration will you be led to?
 - b. Discuss the realities/practicalities of your approach in (i) and (ii) above, i.e. discuss the impact of heat removal, fission product containment, fuel damage and overall plant economics on your design (core configuration).

Do not spend more than an hour on this problem.